# The improved SIMC method for PI controller tuning

### Chriss Grimholt Sigurd Skogestad NTNU, Trondheim, Norway

Reference: C. Grimholt and S. Skogestad, "The improved SIMC method for PI controller tuning", IFAC-conference PID'12, Brescia, Italy, March 2012



# SIMC PI tuning rule\*

- Look at initial part of step response, Initial slope:  $k' = k/\tau_1$
- One tuning rule! Easily memorized

$$K_c = \frac{1}{k'} \cdot \frac{1}{(\theta + \tau_c)}$$
  
$$\tau_I = \min(\tau_1, 4(\tau_c + \theta))$$

 $\tau_{c} \geq -\theta$  : Desired closed-loop response time (tuning parameter) •For robustness select:  $\tau_{c} \geq \theta$ 



Questions:1. How good is really this rule?2. Can it be improved?



Reference: S. Skogestad, "Simple analytic rules for model reduction and PID controller design", *J.Proc.Control*, Vol. 13, 291-309, 2003 (Also reprinted in MIC)
(\*) "Probably the best simple PID tuning rule in the world"

### 1. How good is really the SIMC rule?

Need to compare with:

 Optimal PI-controller for class of first-order with delay processes



# **Optimal controller**

- Tradeoff between
  - Output performance High controller gain ("tight control")

Low controller gain ("smooth control")

- Robustness
- Input usage
- Noise sensitivity
- Quantification
  - Output performance:
    - Frequency domain: weighted sensitivity ||W<sub>p</sub>S||
    - Time domain: IAE or ISE for setpoint/disturbance
  - Robustness: M<sub>s</sub>, GM, PM, Delay margin
  - Input usage: ||KSG<sub>d</sub>||, ISE or TV for step response
  - Noise sensitivity: ||KS||, etc.

Our choice:

**J** = avg. IAE for setpoint/disturbance



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# Output performance (J)



$$J(c) = 0.5 \frac{IAE_{ys}(c)}{IAE_{ys}^{o}} + 0.5 \frac{IAE_{d}(c)}{IAE_{d}^{o}}$$

IAE<sup>o</sup><sub>ys</sub>: PI-optimal for setpoint ( $M_s = 1.59$ )

IAE<sup>o</sup><sub>d</sub>: PI-optimal for disturbance ( $M_s = 1.59$ )

IAE = Integrated absolute error =  $\int |y-y_s| dt$ , for step change in  $y_s$  or d

Cost J is independent of:

- 1. process gain k
- 2. disturbance magnitude
- 3. unit for time

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### Optimal PI-controller: Minimize J for given M<sub>s</sub>



$$\begin{split} \min_{c} J(c)|_{M_{s}=m} \\ \text{PI-controller: } c(s) &= K_{c} \left(1 + \frac{1}{\tau_{I}s}\right) \\ \text{First-order with delay processes: } g(s) &= \frac{k}{\tau_{1}s+1}e^{-\theta s} \\ \theta &= 1, \tau_{1}/\theta = [0, \infty] \\ m &= [..., 1.2, 1.59, 1.7, 2...] \end{split}$$

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**Optimal PI-controller** 





i

Setpoint change at t=0, Input disturbance at t=20,  $g(s)=k e^{-\theta s}/(\tau_1 s+1)$ , Time delay  $\theta=1$ 

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#### **Optimal PI-controller**



Setpoint change at t=0, Input disturbance at t=20,  $g(s)=k e^{-\theta s}/(\tau_1 s+1)$ , Time delay  $\theta=1$ 



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**Optimal PI-controller** 

i



Setpoint change at t=0, Input disturbance at t=20, g(s)=k  $e^{-\theta s}/(\tau_1 s+1)$ , Time delay  $\theta=1$ 



 $M_{s} = 1.2$ 

### Optimal performance (J) vs. M<sub>s</sub>



### Input usage (TV) increases with M<sub>s</sub>



$$TV(u) = \int_0^\infty \left| \frac{du}{dt} \right| dt = \sum_{i=1}^\infty |u_i - u_{i-1}|$$

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## Setpoint / disturbance tradeoff



### Setpoint / disturbance tradeoff

Table 1. Optimal PI-controllers	$(M_s = 1.59)$	and corresponding	IAE-values for	four processes.
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Process	Setpoint		Input disturbance		Optimal combined (minimize $J$ )							
	$K_c$	$ au_I$	$LAE_{ys}^{o}$	K <sub>c</sub>	$ au_I$	$IAE_d^\circ$	$K_c$	$ au_I$	$IAE_{ys}$	$IAE_d$	J	$M_s$
$e^{-s}$	0.20	0.32	1.607	0.20	0.32	1.607	0.20	0.32	1.607	1.607	1	1.59
$\frac{e^{-s}}{s+1}$	0.54	1.10	2.083	0.50	1.0	2.036	0.54	1.10	2.083	2.041	1.00	1.59
$\frac{e^{-s}}{8s+1}$	4.0	8	2.169	3.34	3.7	1.135	3.46	4.0	3.111	1.158	1.23	1.59
$\frac{e^{-s}}{s}$	0.50	$\infty$	2.169	0.40	5.8	15.09	0.41	6.3	4.314	15.4	1.51	1.59

 $IAE_{ys}$  is for a unit setpoint change.  $IAE_d$  is for a unit input disturbance.

Optimal setpoint: No integral action



## Comparison with SIMC

$$K_c = \frac{1}{k'} \cdot \frac{1}{(\theta + \tau_c)}$$
  
$$\tau_I = \min(\tau_1, 4(\tau_c + \theta))$$

Tuning parameter:  $\tau_c$ 

Tight control with good robustness: Select  $\tau_c = \theta$  (effective delay)

• Gives  $M_s$  between 1.59 and 1.7



#### 16 Comparison of J vs. M<sub>s</sub> for optimal and SIMC for 4 processes



### Conclusion (so far): How good is really the SIMC rule?

- Varying  $\tau_{C}$  gives (almost) Pareto-optimal tradeoff between performance (J) and robustness (M<sub>s</sub>)
- $\tau_{\rm C} = \theta$  is a good "default" choice
- Not possible to do much better with any other PIcontroller!
- Exception: Time delay process



### 2. Can the SIMC-rule be improved?

### Yes, possibly for time delay process

$$K_c = \frac{1}{k'} \cdot \frac{1}{(\theta + \tau_c)}$$
  
$$\tau_I = \min(\tau_1, 4(\tau_c + \theta))$$

Tuning parameter:  $\tau_c$ 

Time delay process,  $g = k' e^{-\theta s}$ : SIMC-rule gives integrating controller ( $\tau_I = \tau_1 = 0$ )



# **Optimal PI-settings**



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### Optimal PI-settings (small $\tau_1$ )



### Improved SIMC-rule: Replace $\tau_1$ by $\tau_1 + \theta/3$

$$K_c = \frac{1}{k} \cdot \frac{\tau_1 + \frac{\theta}{3}}{(\theta + \tau_c)}$$
  
$$\tau_I = \min(\tau_1 + \frac{\theta}{3}, 4(\tau_c + \theta))$$

Tuning parameter:  $\tau_c$ 

Time delay process  $(\tau_1 = 0)$ :  $\tau_I = \frac{\theta}{3}$ 



### Step response for time delay process



### <sup>23</sup>Comparison of J vs. Ms for optimal and SIMC for 4 processes



# Conclusion

**Questions:** 

- 1. How good is really the SIMC-rule?
  - Answer: Pretty close to optimal, except for time delay process
- 2. Can it be improved?
  - Yes, to improve for time delay process: Replace  $\tau_1$  by  $\tau_1$ + $\theta$ /3 in rule to get "Improved-SIMC"
- Not possible to do much better with any other PIcontroller!

Reference: C. Grimholt and S. Skogestad, "The improved SIMC method for PI controller tuning", IFAC-conference PID'12, Brescia, Italy, March 2012



# <sup>25</sup> Model from closed-loop response with P-controller

