

# Model-Based Optimization of Economical Grade Changes for the Borealis Borstar<sup>®</sup> Polyethylene Plant

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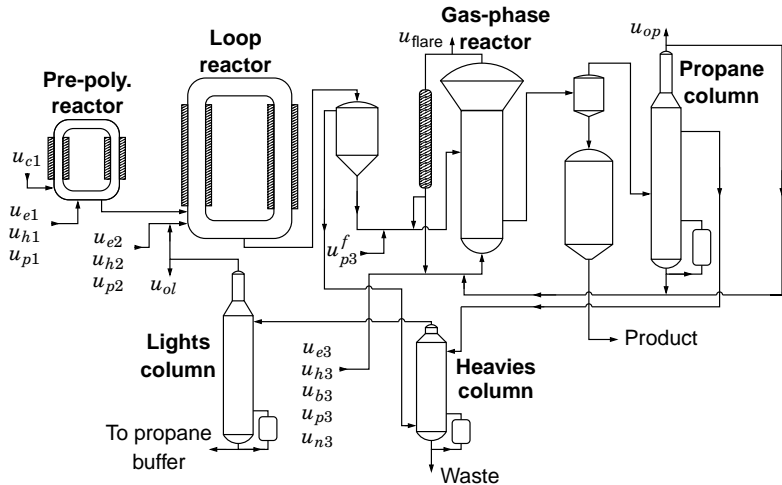
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# Background

- ▶ Polyethylene
  - ▶ Most widely used plastic in the world
  - ▶ Several different grades, i.e., types
  - ▶ Specified by quality variables:
    - ▶ density
    - ▶ melt index
    - ▶ molecular weight distribution
    - ▶ ...
- ▶ Why Grade Changes?
  - ▶ Market demands
  - ▶ Raw material and product pricing
  - ▶ Technology supports several grades
- ▶ How to Perform a Grade Change
  - ▶ Manipulate inflows of raw material in a continuous manner
    - ▶ No “stop-and-go”
  - ▶ Desired: Economically optimal
  - ▶ Obey safety and constraints on e.g., flows, conc., grades.

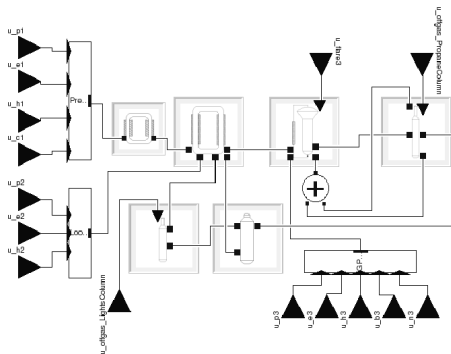
# PE3 at Borealis AB, Stenungsund



- ▶ Inflows: catalyst, ethylene, hydrogen, propane and nitrogen
- ▶ Outflows: propane, off-gases, flare, product, (and waste)

# Modelica Model and Model Size

- ▶ Modelica library constructed



- ▶ Number of

- ▶ states  $\mathbf{x}$ : 46
- ▶ algebraic variables  $\mathbf{w}$ : 167
- ▶ inputs  $\mathbf{u}$ : 15
- ▶ equations in  $\mathbf{F}(\cdot)$ : 213
- ▶ quality variables  $\mathbf{y}$ : 7
- ▶ operational variables  $\mathbf{z}$ : 2

$$\mathbf{0} = \mathbf{F}(\dot{\mathbf{x}}, \mathbf{x}, \mathbf{w}, \mathbf{u})$$

$$\mathbf{y} = \mathbf{g}_y(\mathbf{x}, \mathbf{w}, \mathbf{u})$$

$$\mathbf{z} = \mathbf{g}_z(\mathbf{x}, \mathbf{w}, \mathbf{u})$$

$$\mathbf{x}(t_0) = \mathbf{x}_0$$

## Grade Definitions and Prices/Costs

Grade	$\bar{X}_{he1}$	$\overline{MI}_2$	$\overline{MI}_{mix}$	$\bar{\rho}_{mix}$	$\bar{S}_1$	$\bar{S}_2$	$\bar{S}_3$	$E_j$
A	1.00	1.00	1.00	1.000000	1.000	1.000	1.000	1.24
B	0.37	6.50	3.51	1.001065	1.000	1.132	0.917	1.46
$\pm\%$	$\pm 5$	$\pm 5$	$\pm 5$	$\pm 0.1$	$\pm 0.5$	$\pm 0.5$	$\pm 0.5$	-

- ▶ Grade definitions have *target values* and *intervals*.
- ▶ Inside intervals = *on-grade*  $\Rightarrow$  sell price  $E_j$ .
- ▶ Outside intervals = *off-grade*  $\Rightarrow$  sell price  $E_{off}$ .
- ▶ Costs  $C_i$  of inflows, offgas sell price  $E_{og}$  and off-grade polymer sell price  $E_{off}$ .

$C_c$	$C_e$	$C_h$	$C_b$	$C_p$	$C_n$	$E_{og}$	$E_{off}$
214.6	1.000	8.003	1.419	0.501	0.044	0.266	0.880

# Stationary Optimization Problem

- ▶ Instantaneous profit  $R_j$  in stationarity production of grade  $j$

$$\begin{aligned}
 R_j = & \overbrace{E_j w_{s3}}^{\text{production revenue}} + \overbrace{E_{og} u_{ol} + E_{og} u_{op}}^{\text{offgas revenue}} + \overbrace{C_p w_{p6}^b}_{\text{propane revenue}} \\
 & - \underbrace{\sum_{i \in \{c, e, h, p\}} C_i u_{i1} - \sum_{i \in \{e, h, p\}} C_i u_{i2} - \sum_{i \in \{e, h, b, p, n\}} C_i u_{i3} - C_p u_{p3}^f}_{\text{inflow costs}}
 \end{aligned}$$

- ▶ Optimization problem solved using JModelica.org

$$\max_{\dot{\mathbf{x}}, \mathbf{x}, \mathbf{w}, \mathbf{u}} R_j$$

$$\text{s.t. } \mathbf{0} = \mathbf{F}(\dot{\mathbf{x}}, \mathbf{x}, \mathbf{w}, \mathbf{u}) \quad (\text{dynamics})$$

$$\mathbf{y}_j = \mathbf{g}_y(\mathbf{x}, \mathbf{w}, \mathbf{u}) \quad (\text{on specification})$$

$$\mathbf{z}_j = \mathbf{g}_z(\mathbf{x}, \mathbf{w}, \mathbf{u}) \quad (\text{pressures in GPR})$$

$$\dot{\mathbf{x}} = \mathbf{0} \quad (\text{stationarity})$$

$$\mathbf{x}_{\min} \leq \mathbf{x} \leq \mathbf{x}_{\max}, \mathbf{w}_{\min} \leq \mathbf{w} \leq \mathbf{w}_{\max}, \mathbf{u}_{\min} \leq \mathbf{u} \leq \mathbf{u}_{\max}$$

## Stationary Optimization – Some results

- ▶ Specifications on grade variables sets reactant ratios.
- ▶ Profitable to produce  $\Rightarrow$  production level at maximum.
- ▶ Off-gases at minimum and flare closed.
- ▶ Minimizes expensive components in off-gases.
- ▶ Gives economically optimal operating points for grade  $j$ .

## Dynamic Optimization – Ideal Profit

- ▶ Ideal instantaneous profit  $R_j$  for grade  $j$

$$R_j = \overbrace{\left( (E_j - E_{\text{off}})\theta_j(\mathbf{y}) + E_{\text{off}} \right)}^{\text{Effective sell price}} w_{s3} + E_{og}u_{ol} + E_{og}u_{op} + C_p w_{p6}^b \\ - \sum_{i \in \{c, e, h, p\}} C_i u_{i1} - \sum_{i \in \{e, h, p\}} C_i u_{i2} - \sum_{i \in \{e, h, b, p, n\}} C_i u_{i3} - C_p u_{p3}^f,$$

where  $\theta_j(\mathbf{y})$  is the ideal on-grade function for grade  $j$

$$\theta_j(\mathbf{y}) = \begin{cases} 1 & \text{if } y_{ji}^{\min} \leq y_i \leq y_{ji}^{\max}, \quad i \in \{1, \dots, 7\} \\ 0 & \text{otherwise,} \end{cases}$$

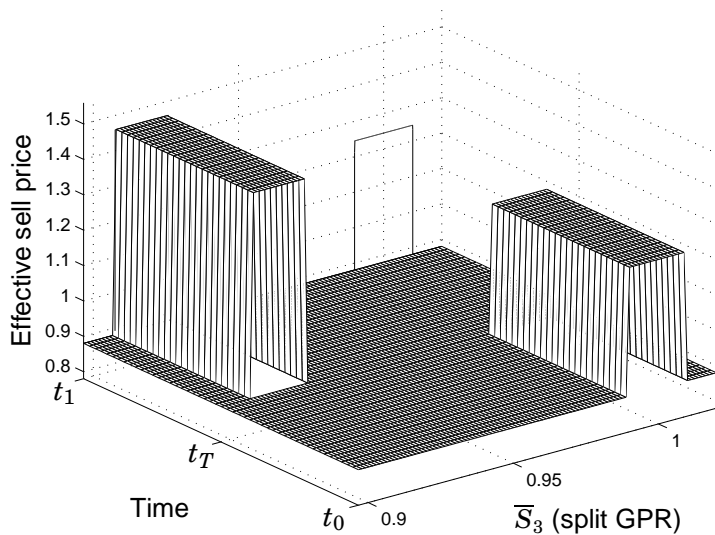
- ▶ Define a time interval  $[t_0, t_1]$  and a transition time  $t_T$

$$R = \begin{cases} R_A, & t_0 \leq t \leq t_T \\ R_B, & t_T < t \leq t_1. \end{cases}$$

- ▶ **Goal:** Maximize cumulative profit  $V_{\text{eco}} = \int_{t_0}^{t_1} R dt$ .



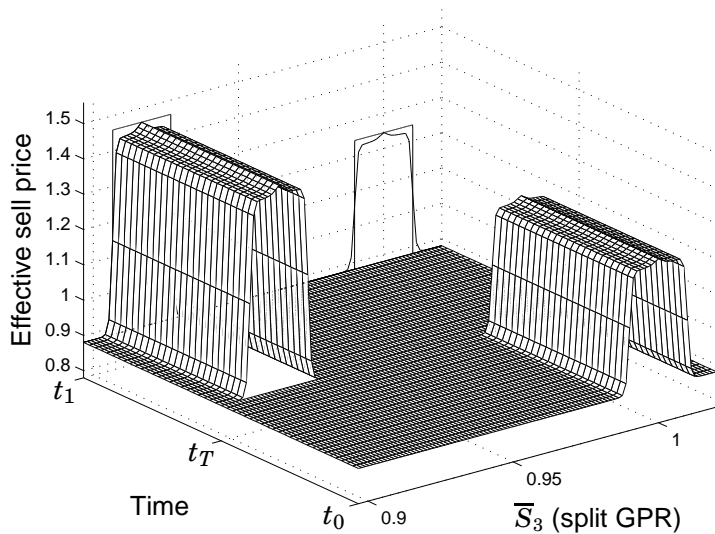
# Ideal Effective Sell Price – Visualization



# Dynamic Optimization – Difficulties and a Solution

- ▶ Difficulties
  - ▶ Cost function is *not differentiable*.
  - ▶ Might be optimal to be on quality variable *interval border*.
  - ▶ Desired to be *on-target* with grade variables.
  - ▶ Desired to be *on-target* with operational variables.
- ▶ A solution
  - ▶ *Smooth* approximation of ideal on-grade function  $\theta_j(\mathbf{y})$ .
  - ▶ *Economical* incentives, i.e., “price peaks” at target values.
  - ▶ Rational function of
    - ▶ grade variables
    - ▶ target values
    - ▶ grade intervals
  - ▶ Parameters in rational function control
    - ▶ Smoothness
    - ▶ Price peak

# Smooth approximation with peaks – Visualization



# Dynamic Optimization Problem

$$\max_{\dot{\mathbf{u}}} \int_{t_0}^{t_1} \left( \tilde{R} - \dot{\mathbf{u}}^T \mathbf{U}_d \dot{\mathbf{u}} \right) dt$$

$$\text{s.t. } \mathbf{0} = \mathbf{F}(\dot{\mathbf{x}}, \mathbf{x}, \mathbf{w}, \mathbf{u}), \quad \mathbf{u} = \int_{t_0}^t \dot{\mathbf{u}} d\tau$$

$$\mathbf{y} = \mathbf{g}_y(\mathbf{x}, \mathbf{w}, \mathbf{u})$$

$$\mathbf{z} = \mathbf{g}_z(\mathbf{x}, \mathbf{w}, \mathbf{u})$$

$$\mathbf{x}_{\min} \leq \mathbf{x} \leq \mathbf{x}_{\max}, \quad \mathbf{w}_{\min} \leq \mathbf{w} \leq \mathbf{w}_{\max}$$

$$\mathbf{u}_{\min} \leq \mathbf{u} \leq \mathbf{u}_{\max}, \quad \mathbf{y}_{\min} \leq \mathbf{y} \leq \mathbf{y}_{\max}$$

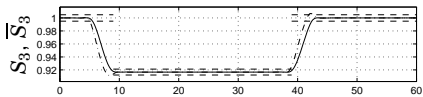
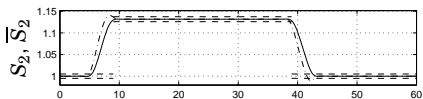
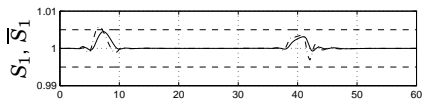
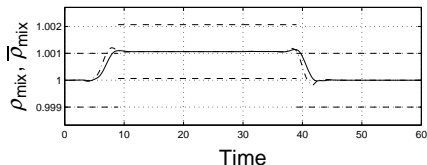
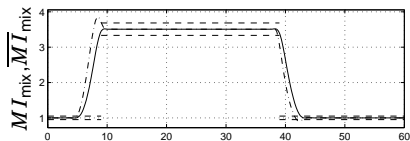
$$\mathbf{z}_{\min} \leq \mathbf{z} \leq \mathbf{z}_{\max}, \quad \dot{\mathbf{u}}_{\min} \leq \dot{\mathbf{u}} \leq \dot{\mathbf{u}}_{\max}$$

$$\mathbf{x}(t_0) = \mathbf{x}_s, \quad \mathbf{u}(t_0) = \mathbf{u}_s$$

$$\mathbf{u} = \mathbf{u}_e, \quad t_1 - T_c \leq t \leq t_1$$

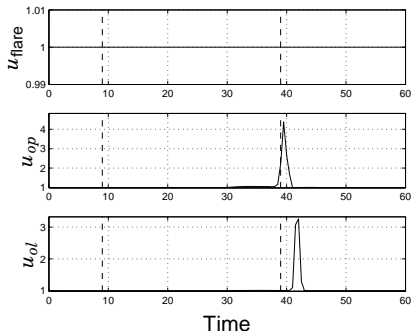
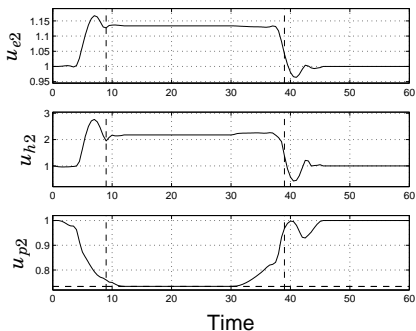
- ▶ Control flow derivatives  $\dot{\mathbf{u}}$  as decision variables.
- ▶  $\dot{\mathbf{u}}^T \mathbf{U}_d \dot{\mathbf{u}}$  penalizing highly varying control flows.
- ▶ Control flows fixed at an end interval, avoiding all fresh inflows closing.
- ▶ Solved using JModelica.org.

# Results – Quality variables



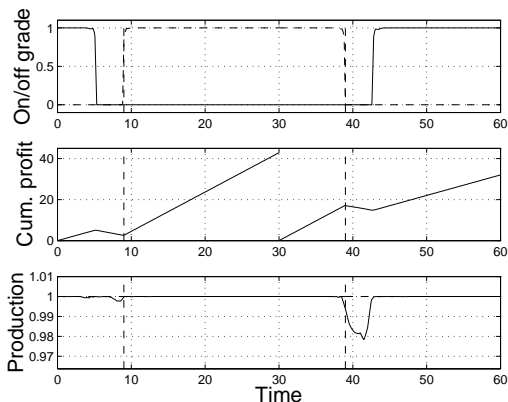
- ▶ Economical incentive for on-target production large enough.
- ▶ Over-/undershoots in instantaneous quality variables.
- ▶ Preparations performed prior grade change.

## Results – Control flows



- ▶ Change for a longer time period than off-grade period.
- ▶ Significant over-/undershoots for rapid grade change.
- ▶ Flare never used due to pure economical loss.
- ▶ Off-gases remove hydrogen at economically beneficial times.

## Results – Production and Profit



- ▶ Most profitable product produced the longest time.
- ▶ High production rate  $\Rightarrow$  small reactor hold-up times.
- ▶ Economically optimal transition has three phases:
  1. Preparation
  2. Transition
  3. Completion

# Summary

- ▶ A Modelica library has been constructed for the Borealis Borstar<sup>®</sup> Polyethylene Plant.
- ▶ Cost functions for optimization of economical grade changes have been designed.
- ▶ Economically optimal grade changes have been characterized.